# An Overview of ISA 84 Standard for Safety Instrumented Systems (SIS) and the Safety Life Cycle

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ISA 84 Safety Instrumented Systems and the Safety Life Cycle

Agenda:

- Safety components, acronyms, and definitions
- ANSI/ISA 84.00.01 Standard for Safety Instrumented Systems
- Safety Life Cycle
- Incorporating safety systems into process design
- Workshop



### • Components:

- OSafety Instrumented Function (SIF)
- OSafety Instrumented System (SIS)
- OSafety Integrity Level (SIL)
- OSafety Requirement Specification (SRS)
- OSafety Life Cycle
- OIndependent Protection Layer (IPL)



#### SIF – Safety Instrumented Function

 Individual interlock or automatic trip function that is designed to alleviate or minimize an undesired hazard, as determined in the PHA/HAZOP and the SIL Selection/LOPA

 Includes all instrumentation in the interlock function, from the sensor and transmitter through the control system all the way to the final element (e.g., isolation valve)



#### SIS – Safety Instrumented System

- A critical system that consists of one or more automatic Safety Instrumented Functions (SIFs) or interlocks
  - Example: Fired Heater burner management system (BMS)





#### SIL – Safety Integrity Level Risk reduction levels:

SIL	RRF	PFD (1/RRF)	
0	0-10	≥10 <sup>-1</sup>	
1	>10 to ≤100	≥10 <sup>-2</sup> to <10 <sup>-1</sup>	
2	>100 to ≤1000	≥10 <sup>-3</sup> to <10 <sup>-2</sup>	
3	>1000 to ≤10,000	≥10 <sup>-4</sup> to <10 <sup>-3</sup>	
4	>10,000 to ≤100,000	≥10 <sup>-5</sup> to <10 <sup>-4</sup>	



### SIL – Safety Integrity Level

OLevel of risk reduction that a SIF must achieve

- <u>Target / Required SIL</u> amount of risk reduction determined as a need during PHA / HAZOP and then the level is determined during a simplified SIL Selection or elaborate LOPA (Layer of Protection Analysis)
- <u>Achieved / Verified SIL</u> calculated risk reduction utilizing Markov equations and includes all components of the interlock to determine the level of risk reduction (RRF) or 1/PFD (Probability of Failure on Demand)



SIL – Safety Integrity Level

Levels of risk:

○ SIL o (none) – tolerable risk

○ SIL 1 – minimal risk

95% of all SIL-rated interlocks

○ SIL 2 – medium risk

Less than 5% of all SIL-rated interlocks

- SIL 3 high risk
  - Less than 1% of all SIL-rated interlocks (typically found in the nuclear industry or off-shore platforms)

○ SIL 4 – highest risk (not likely in petroleum or chemical industry)



#### SRS – Safety Requirement Specification

- Document containing detailed SIS interlock information
- Safety Life Cycle
  - Activity designed to include all phases of the life of a SIF and SIS
    - *KEY NOTE*: It's not enough to just *install* a SIS. It must be properly designed and maintained so it is available when the need arises!!!

 ANSI/ISA 84 and Safety Life Cycle were developed to guide a safety system from the Risk Assessment "cradle" to the Decommissioning "grave".

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# ANSI/ISA 84.00.01 Standard for SIS

- ANSI/ISA 84.00.01 Application of Safety Instrumented Systems (SIS) for Process Industries :
  - Follows IEC 61511
  - First version in 1996
  - Second version approved in 2004 (included a "Grandfather Clause")
  - OSHA recognizes this standard as a RAGAGEP
  - Defines Safety Instrumented System (SIS)
  - Defines all phases required in Safety Life Cycle



# ANSI/ISA 84 and Safety Life Cycle



- Accidents/Incidents can and do occur, so in order to help minimize the frequency and/or severity -
- Safety Instrumented Systems and Safety Life Cycle are designed to minimize risk
- But if the Safety Life Cycle is stopped, this could occur...







- 15 fatalities and 180 injuries that day in 2005
- Resulted in multitude of citations with a hefty fine of \$21MM
- 2009 Follow-up FTA inspection was conducted and \$87MM fine was given; most of the FTAs related to PSVs and SIS



- Due to public concern over the severity of the 2005 BP Texas City incident, OSHA initiated NEP (National Emphasis Program) inspections in petroleum refineries across the country in 2007
  - OSHA included SIS analysis in the NEP dynamic list for refineries (due to SIS and instrumentation failures considered as contributing causes of the BP incident)
  - OSHA more recently initiated a nationwide NEP directive for chemical facilities with PSM-covered chemicals in late 2011



- ANSI/ISA 84.00.01 Application of Safety Instrumented Systems (SIS) for Process Industries:
  - OSHA recognizes this standard as RAGAGEP (Recognized and Generally Accepted Good Engineering Practice) and has considered it to be within the scope of OSHA 1910.119 PSM regulation under Mechanical Integrity (MI)



## **Protection Layers**

#### IPL – Independent Protection Layer

• Protective items, when used alone or in combination with diverse types, that are meant to reduce risk to personnel, the environment, or property

• Examples: BPCS (control system), alarms and operator response, SIS, physical devices (PSVs, dual seals, dikes, flares, deluges, etc.), and other human mitigation (emergency response)



## **Protection Layers**

Process Hazards/Risk and IPLs (ups and downs)





### **Protection Layers**

Emergency Response (Plant and then Community)

Mitigation (SIS, mechanical mitigation)

Prevention (Alarms w/ intervention, mechanical protection)

**BPCS** 

PROCESS



## Protection Layers / SIFs / SISs

- Safety systems/interlocks are a vital protection layer between the hazards of the process and the public when inherent design is not enough
- Safety Systems are added to the process design to minimize these risks to a tolerable level or ALARP (As Low As Reasonably Practical)





- SIF/SIS is added to a design during the "cradle" stage or PHA as a safeguard to mitigate or minimize a hazard
- Each SIF is assigned a Safety Integrity Level (SIL) during the SIL Analysis or LOPA risk assessment
  - ○SIL o lowest risk
  - ○SIL 4 highest risk
- Each incremental SIL must be more reliable and available to operate when required (thus installation and maintenance costs increase)



- Requirements when designing SIS:
  - Separation:
    - Instrumentation interlock instrumentation CAN NOT be part of control logic
    - Safety Control System requires safety logic solver that segregates its inputs and outputs
  - Robust equipment options:
    - Examples:
      - Honeywell ST3000 Safety transmitter with HART 6.0
      - MAXON MM/MA series safety isolation valves
      - DeltaV Redundant SLS



- Reliability and availability can also be achieved by:
  Architecture
  - Using redundancy and voting logic of the initiators, safety control system, and/or final elements (e.g., 1002, 2003 required to achieve safe state)
  - ○Installation per manufacturer's guidelines
  - Testing / Validation and Replacement both at initial startup as well as at specified testing intervals or after any modification (i.e., via PSSR)



• When designing or modifying a SIS, keep in mind there are two types of failures:

- Safe Failures
- Dangerous Failures

Safe Failures are the desired failure

- Initiated (actual event)
- Spurious (false undesired but still safe)
- Dangerous failures are not desired
  - Inhibited (bypassed)
  - Dangerous operation (doesn't trip when needed)



# Safety Systems Design – Voting Logic

• How to design for safe failures without dangerous failures or with minimal spurious trips?



# Safety Systems Design - SIL Verification

- SIL verification involves multiple Morkov model calculations to determine the achieved SIL range
- Interlock component data used for verification:
  MTTFS
  - PFD<sub>avg</sub>
  - RRF (inverse of PFD or 1/PFD)
  - $\bigcirc \beta \%$  (when using multiple components)
  - $\bigcirc \lambda_{du}$  (undetected dangerous failures)
  - $\bigcirc \lambda_{sp}$  (safe or spurious failures)



# Safety Systems Design - SIL Verification

Safety	Safety Instrumented System Performance Requirements			
Integrity Level (SIL)	Safety Availability Required	Average Probability of Failure on Demand (PFDavg)	Risk Reduction Factor (RRF) RRF=1/PFD	
1	90.00 - 99.00 %	10 <sup>-1</sup> to 10 <sup>-2</sup>	10 to 100	
2	99.00 - 99.90 %	10 <sup>-2</sup> to 10 <sup>-3</sup>	100 to 1,000	
3	99.90 – 99.99 %	10 <sup>-3</sup> to 10 <sup>-4</sup>	1,000 to 10,000	



# Safety Systems Design - SIL Verification

- If the required SIL can not be achieved with the initial design, some options are:
  - More frequent proof testing
  - Add redundancy (i.e., initiating device, control system, final element)
  - Install "smarter" device (i.e., HART smart transmitter or transmitter vs. switch or relay, smart control /isolation valve with diagnostics and feedback and position indication vs. basic control valve)
  - OAdd other IPL(s)



# Validation/Functional Proof Testing

- Proof Tests <u>must</u> be performed at the frequency determined during SIL verification (and as stated in the SRS) to validate the reliability of the SIF
  - Many facilities prefer to perform these tests during turnaround, so SIS may be designed to perform between 4-5 year testing frequency
- It should include the following information:
  - Test procedure
  - Date of test and all personnel performing the test
  - Control logic version # (if available)
  - Results of entire test and any abnormalities found



#### General Concepts to Remember in Design

- Separation from control logic
- Two words in design to achieve lower MTTFS (PFD) or higher RRF to achieve the SIL:
  - Diagnostics, diagnostics, diagnostics,...
  - Redundancy
- Transmitters with diagnostics (i.e., HART) can detect problems before going awry or failing, making troubleshooting and repair much easier
- Hence, the desire for transmitters with diagnostics over switches



#### General Concepts to Remember in Design

- If using switch, solenoid, or relay (anything on/off or discrete), verify that it is normally energized during operation (fail safe)
- Use dedicated wiring to each device (as much as possible)
- Minimize common cause failures (i.e., common wires, instrument taps, or same controller or I/O card)
- Mechanical devices are the weakest link in the SIF. They can stick if not moved periodically (i.e., PSVs, valves, switches)
  - To remedy this issue: install dual isolation or modulating valves that can be partially stroked



## Workshop – Fired Heater H-1 P&ID

What voting logic/redundancy options are used in this SIF? (hint: both initiators and final elements)





# Final Review



- Components
  - OIPL
  - **O**SIS
  - **O**SIF
  - **O**SIL
    - Required/ Target SIL
    - Achieved SIL
  - **OSRS**
  - OSafety Life Cycle
    - cradle to grave



# **Final Review**

- Design of the SIF/SIS must be capable of achieving the target SIL
- Design of the SIF/SIS should minimize common cause and dangerous failures
- Employer must continue the Safety Life Cycle timelines as determined in the SRS to the keep the SIF reliable and available to reduce risk
  - Functional Proof Test at a specified interval or after any changes to hardware or software configuration
  - Mission Time hardware replacement interval
  - Document any modifications to SIS or protection layers (MOC)



# Introduction to **PROCESS**

#### **PROCESS** Chemical Engineering Services

- Process Design (FEL-0, 1, 2, and 3)
- O Process Modeling/Simulation (CHEMCAD/Aspen/HYSYS/etc.)
- Operations Support
- O Process Safety Services (PHAs, LOPA, SIL Selection, etc.)

#### The **PROCESS** Competitive Advantage

- The Best Process Engineers Available
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